Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Canceled)

2. (Previously presented) The process according to claim 24, wherein the oxygenates and unsaturates are selected from the group consisting of normal alcohols, mono-olefins, and mixtures thereof.

3. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least 0.5 wt% normal alcohols as oxygenates.

4. (Original) The process of claim 3, wherein the normal alcohols boil in the range of from about 50°C to about 350°C.

5-6. (Canceled)

7. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 5.0 wt % mono-olefins.

8. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 15.0 wt % mono-olefins.

9. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 25.0 wt % mono-olefins.

10. (Original) The process of claim 9, wherein the mono-olefins boil in the range of from about -105 to 350°C.

11. (Previously presented) The process of claim 24, wherein the Fischer-Tropsch hydrocarbon stream is a low-boiling fraction in a range from about -65°C to about 350°C.

12-15. (Canceled)

16. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is from a hydrogen production unit.

17. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is recycled from a hydroprocessing operation.

18. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is syngas.

19-23. (Canceled)

24. (Currently amended) A process for hydroconversion of a Fischer-Tropsch hydrocarbon stream including oxygenates and hydrocarbon unsaturates with reduction in formation of heavy molecular weight products during heating <u>comprising at least one preheating step prior to a heating step for achieving hydroconversion reaction temperature</u>, the process comprising:

a) adding a first hydrogen-containing gas to the hydrocarbon stream <u>prior to the at least one preheating step and</u> not under hydroconversion conditions, wherein the first hydrogen-containing gas is sufficient to reduce the amount of heavy molecular weight products formed during <u>the preheating</u> ~~heating~~ as compared to a heated hydrocarbon stream without added hydrogen, to form a mixed stream;

b) ~~heating~~ <u>preheating</u> the mixed stream;

c) adding a second hydrogen-containing gas to the preheated ~~heated~~ mixed stream sufficient to effect hydroconversion of the mixed stream, to form a hydroconversion feed stream;

d) heating the hydroconversion feed stream to reaction temperature; and

e) hydroconverting the hydroconversion feed stream.

25. (Original) The process of claim 24, wherein the first hydrogen-containing gas is added in an amount less than about 500 Standard Cubic Feed per Barrel (SCFB).

26. (Original) The process of claim 25, wherein the first hydrogen-containing gas is added in an amount less than about 100 SCFB.

27. (Original) The process of claim 26, wherein the first hydrogen-containing gas is added in an amount less than about 50 SCFB.

28. (Original) The process of claim 24, wherein the second hydrogen-containing gas is added in an amount less than 750 SCFB.

29. (Currently amended) The process of claim 24, wherein the mixed stream is preheated ~~heated~~ to a temperature in the range of from about 120°C to about 400°C.

30. (Currently amended) The process of claim 24, wherein the mixed stream is preheated ~~heated~~ to a temperature in the range of from about 250°C to about 400°C.